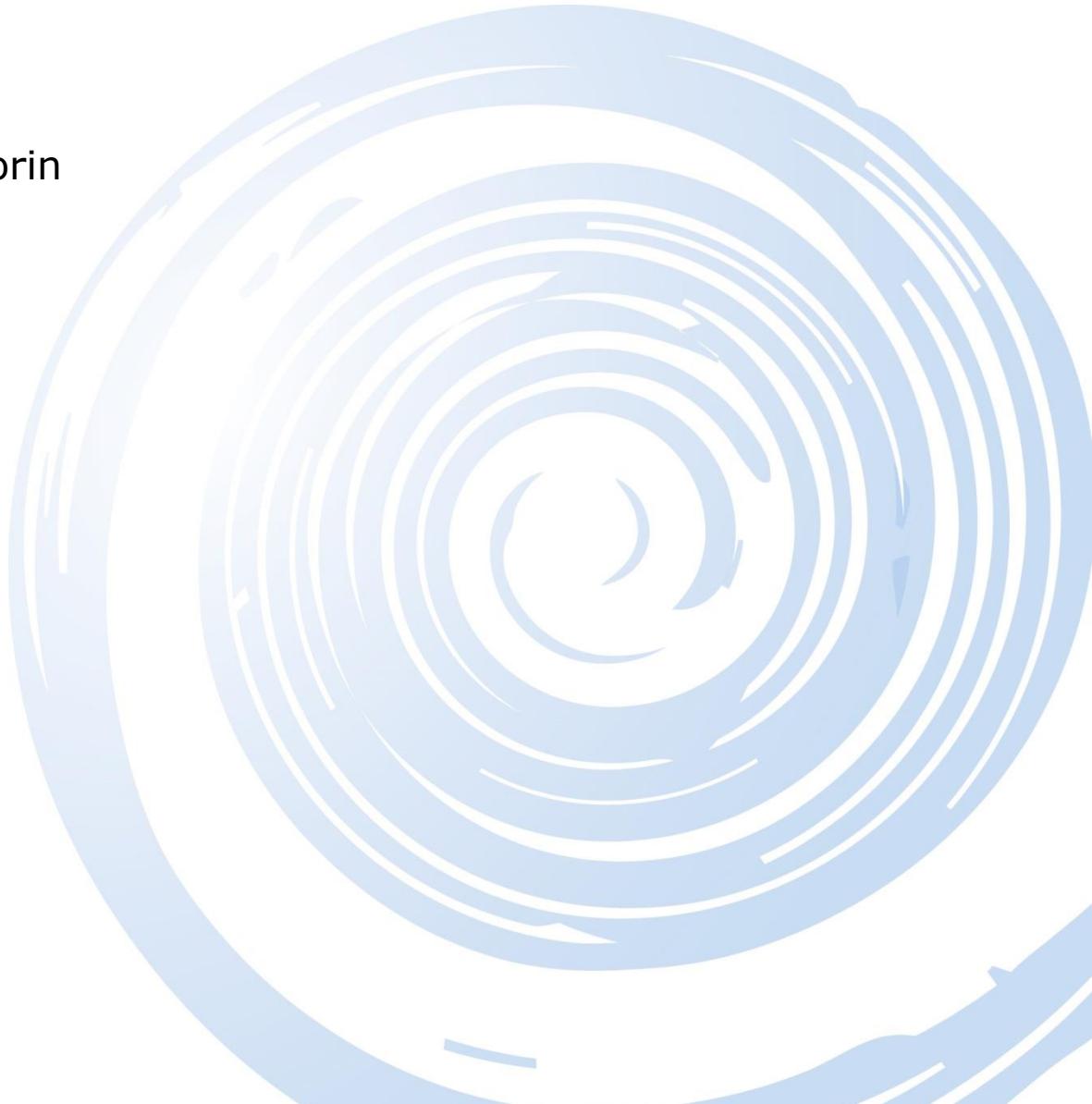


# Aquaporin og DTU Miljø

Agata Zarebska, DTU Miljø

Michael Holm Møller, Aquaporin

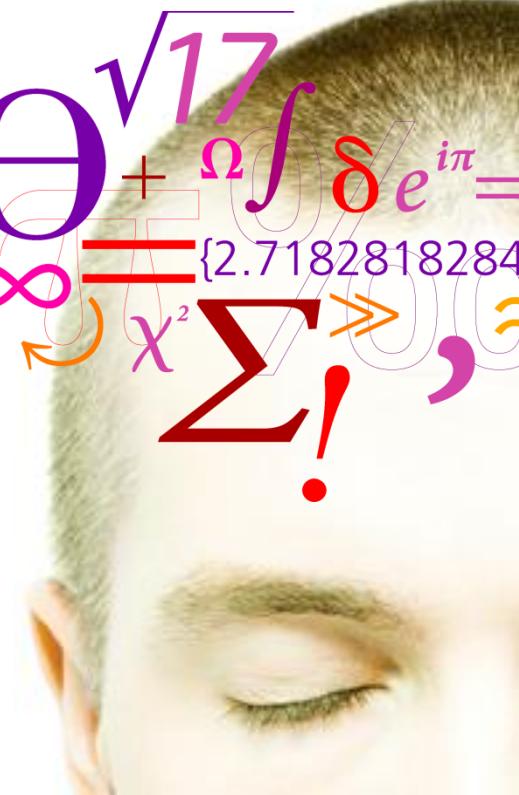


# Combined forward osmosis and membrane distillation

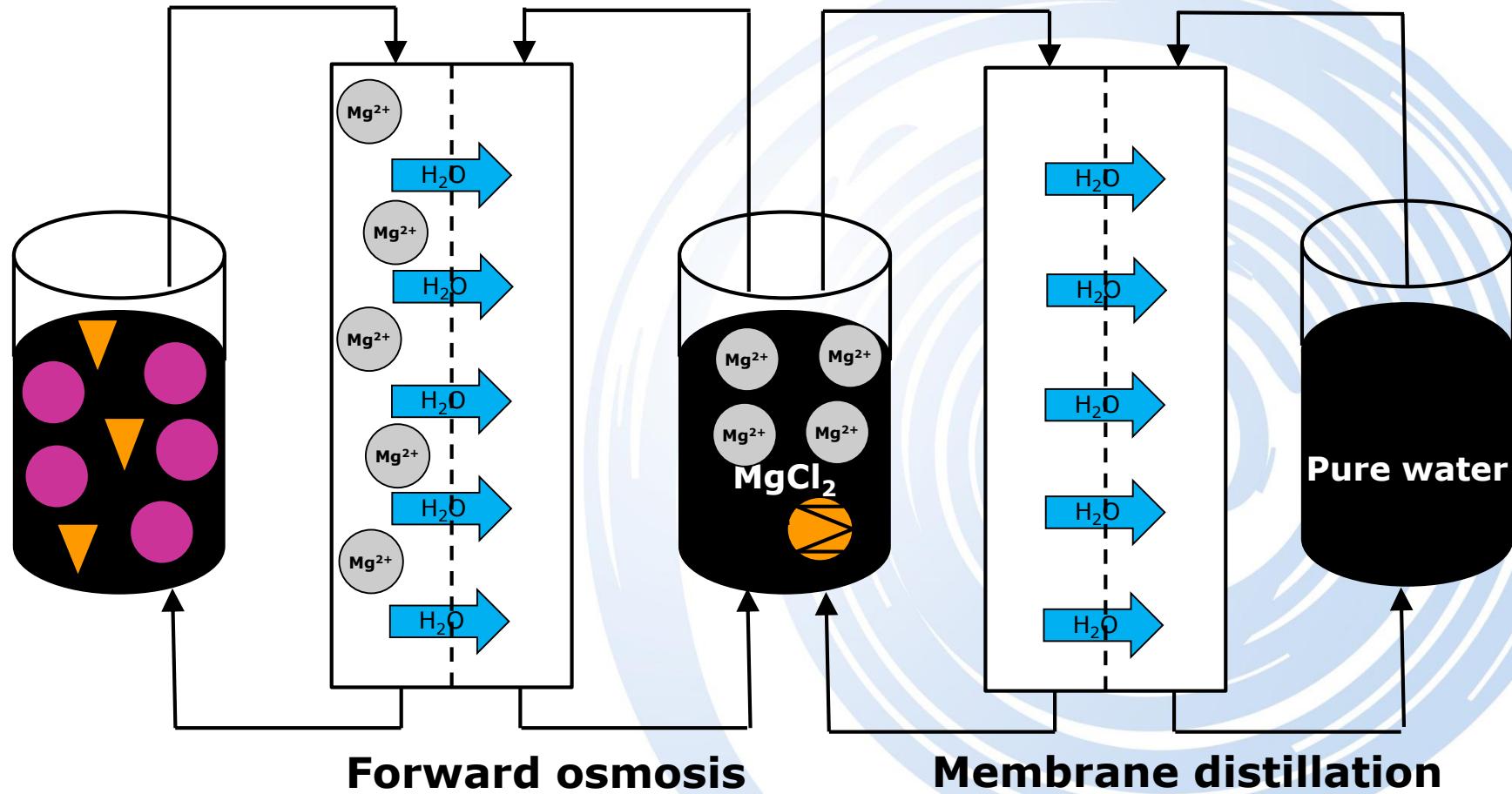
**Agata Zarebska<sup>1</sup>, Jörg Vogel<sup>2</sup>,  
Michael Holm Møller<sup>2</sup>, Oliver  
Geschke<sup>2</sup>, Claus-Helix-Nielsen<sup>1,2</sup>**

<sup>1</sup> Dept. of Environmental Eng.

<sup>2</sup> Aquaporin A/S


$$f(x+\Delta x) = \sum_{i=0}^{\infty} \frac{(\Delta x)^i}{i!} f^{(i)}(x)$$
$$\int_a^b \Theta \delta e^{i\pi} =$$
$$\sqrt{17} + \Omega \int \delta e^{i\pi} =$$
$$\infty - \{2.7182818284\}$$
$$\Sigma \gg ,$$
$$\Theta !$$

# Hybrid process: Forward osmosis-Membrane Distillation



# Forward Osmosis



## Forward osmosis

- ☺ No need of high hydraulic pressure
- ☺ Reduced fouling & simple cleaning

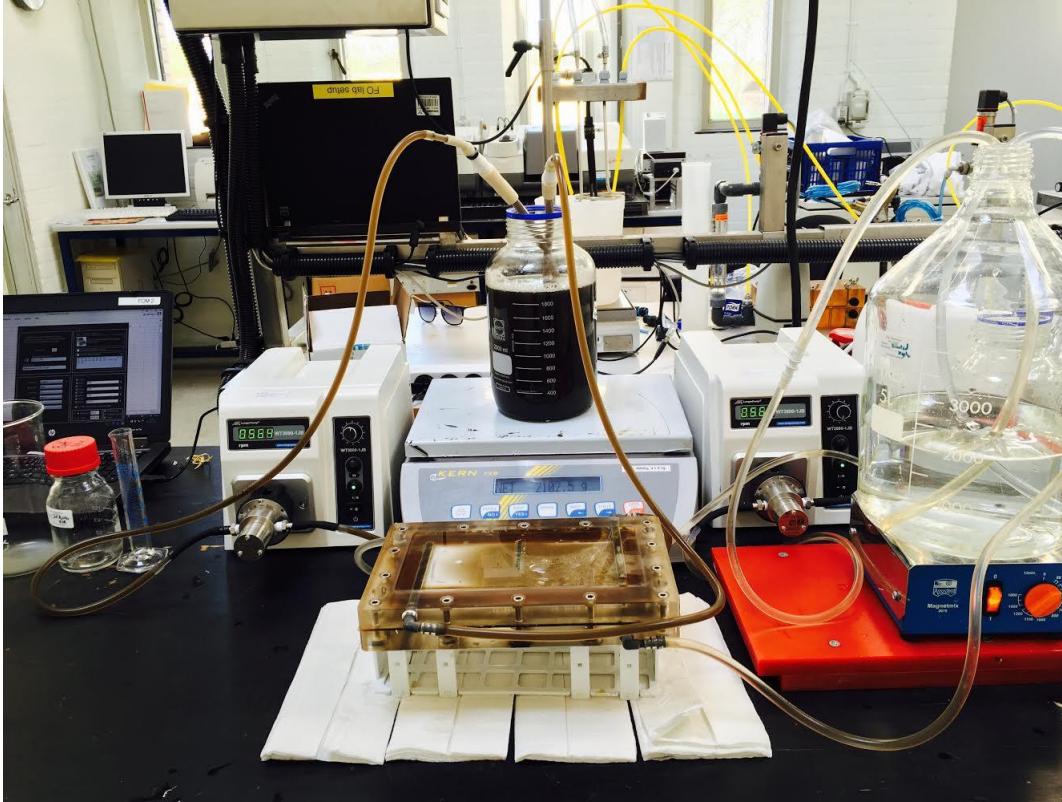
## Membrane distillation

- ☺ Low energy consumption (utilized excess of heat)
- ☺ Water production & draw solution regeneration



## Acknowledgement: *Kuiling Li*

# Forward Osmosis

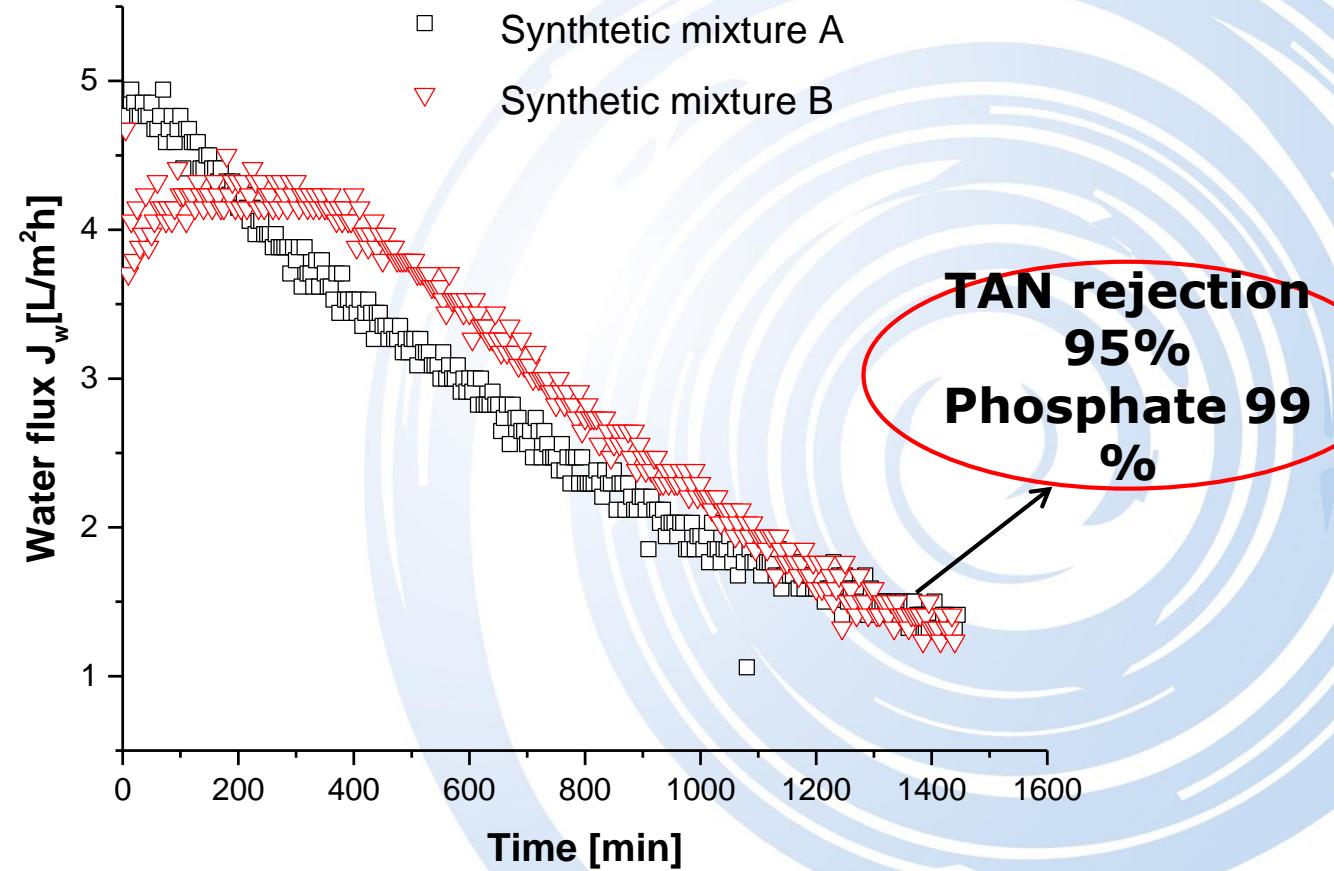


## Operating conditions

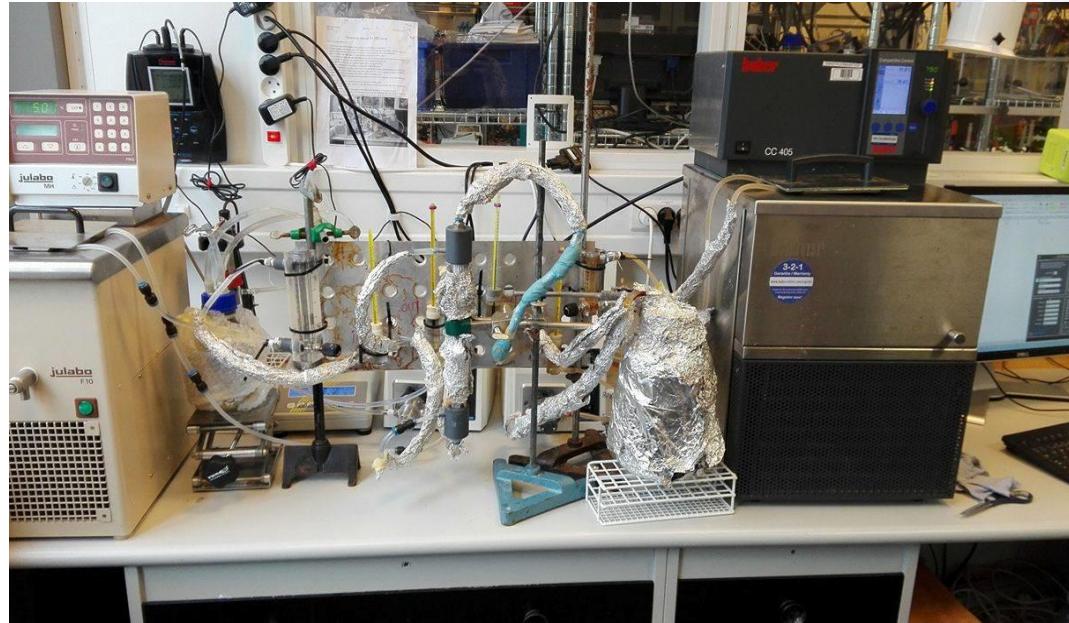
- **Feed:** Synthetic mixture 2L
- **Draw solution:**  $MgCl_2$  0.66 M 2L
- **Membrane:** Aquaporin Inside™
- **Temperature:** 24 °C
- **Experiments time:** 24 h
- **Velocity:** 8.3 cm/s

Acknowledgement: *Rajath Sathyadev Rajmohan*

# Forward Osmosis: Results



# Membrane distillation

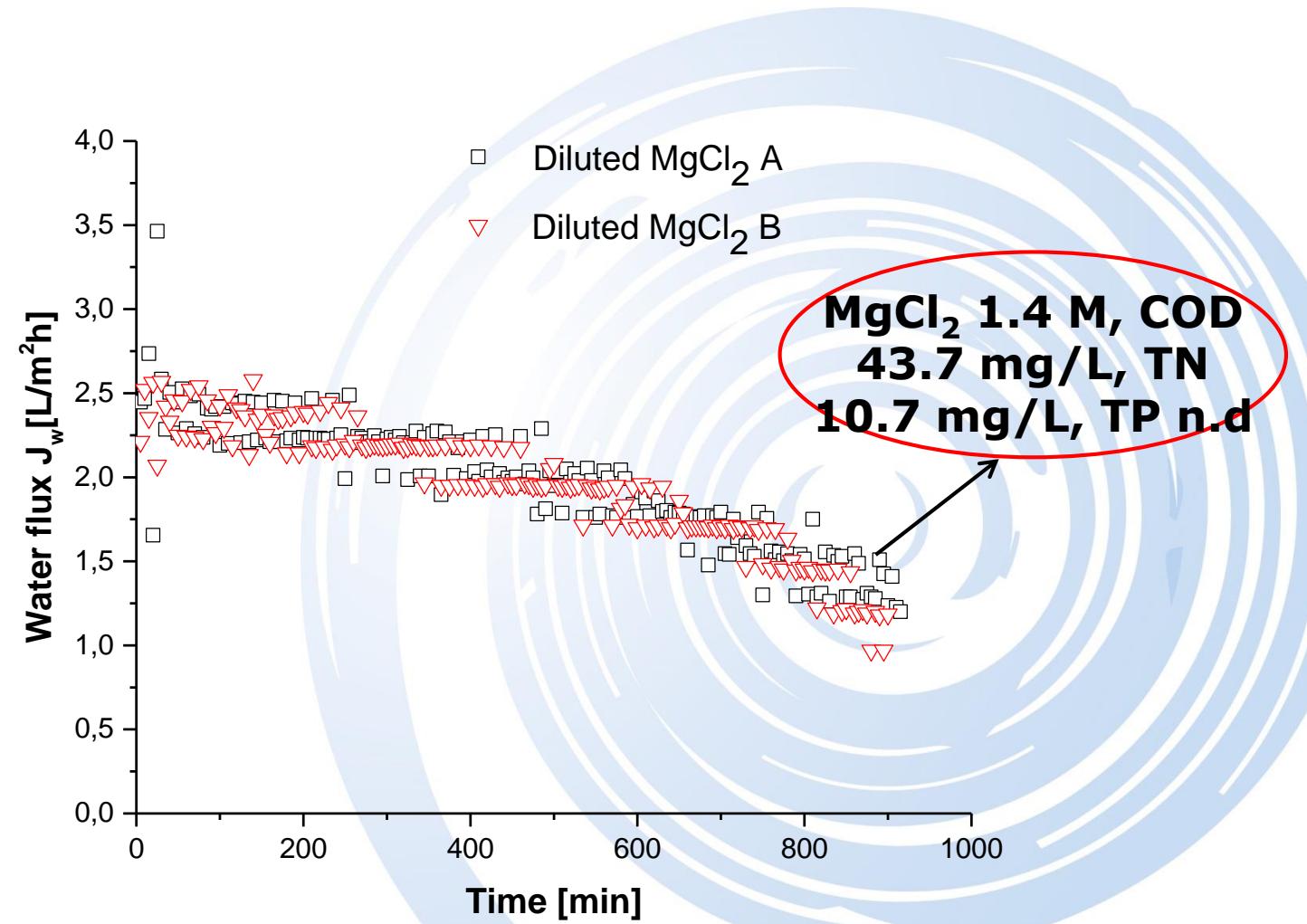


## Operating conditions

- **Feed:** Diluted  $MgCl_2$  (0.43M) coming from FO experiments with synthetic mixture
- **Distillate:** DI water
- **Membrane:** PTFE hollow fibers
- **Temperature Feed<sub>inlet</sub>:** 55 °C
- **Temperature Distillate<sub>inlet</sub>:** 22 °C
- **Velocity Feed:** 0.6 m/s
- **Velocity Distillate:** 0.03 m/s
- **Experiments time:** 15 h

Acknowledgement: *Agnieszka Niedzielska*

# Membrane distillation: Results



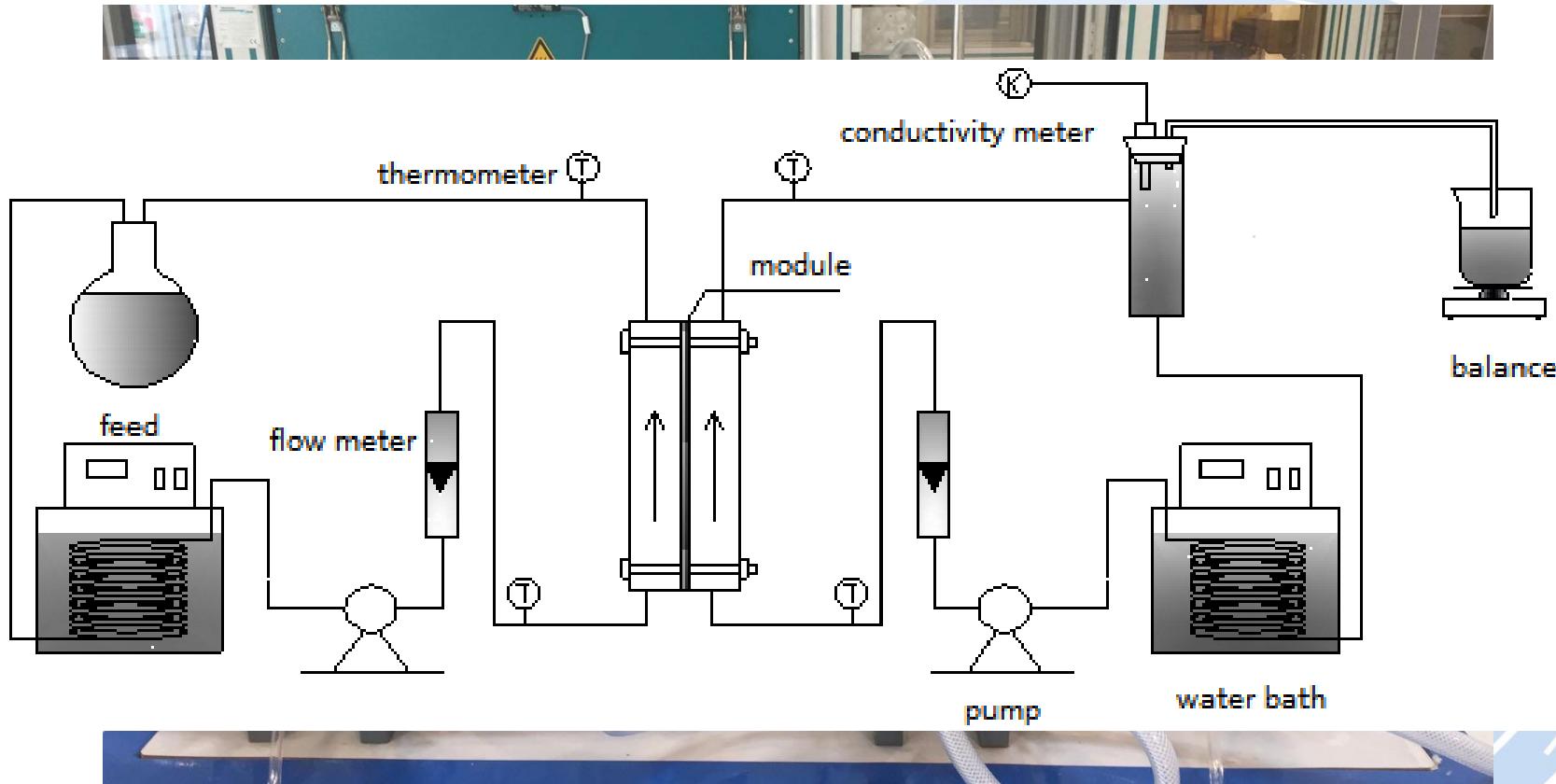
# MEM-FO: progress

		Mid-April	Mid-May	Mid-May	Mid-Juni	Mid-Juni	Mid-Juli	Mid-August	Mid-August	Mid-September
Milestones	Combing FO-MD	Construction of MD setup	x							
	Optimization of operating conditions		x	x	x					
Data evaluation	Conducting experiments		x	x	x					
	Assessing membrane performance				x	x				
Designing pilot plant	Assessing economic feasibility				x	x				
	Designing pilot plant						x			

**Milestone 1:** Water treatment setup built, operational and optimized.

**Milestone 2:** Data analysis, cost evaluation, design pilot plant.

# MEM-FO: progress



## Membrane distillation setup

# MEM-FO: experimental plan

## Starting parameters

- ❖ Temperatures: Feed = 40 ° C / distillate = 20 ° C
- ❖ Module: 1.7x5.5 MiniModule (3M); X-50 PP fibers; active area 0.5 m<sup>2</sup>  
& new developed electospun polyphenylsulfon nanofiber membrane by DTU Energy
- ❖ Feed: MgCl<sub>2</sub> solution

## Parameters to investigate

- ❖ Flux at 20 ° C difference
  - 1M MgCl<sub>2</sub>
  - 1.5M MgCl<sub>2</sub>
- ❖ Flow speed:
  - How slow can we go ? ( $V_{feed}$  <1.6 L/min-2.5 L/min>,  $V_{distillate} \sim 2.5$  L/min)
  - What is the optimal speed (highest flux) ?
  - Change temperature difference to 10 and 30 ° C

# Thank you for your kind attention



## Acknowledgement

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